# Advanced Wet Explosion (AWEx) Pretreatment for making viable biorefineries from lignocellulosic biomass

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### Feedstocks – Washington State



#### **Wheat Straw**

- In Washington state, up to 2 million dry tons is produced per year, could add potential value to the state's economy.
- More than 25,000
   jobs are tied to wheat
   farming in

| Production Zone | Million<br>Metric Tons (MMT) | Million<br>Bushels |
|-----------------|------------------------------|--------------------|
| North Central   | 1,86                         | 68.3               |
| Northeast       | 1.86                         | 68.3               |
| Central         | 1.24                         | 45.6               |
| Southeast       | 0.74                         | 27.3               |
| Southwest       | 0.47                         | 17.1               |
| Northwest       | 0.03                         | 1.0                |
| Total           | 6.20                         | 227.6              |



## Hardwood (e.g. Poplar)

- In USA, 368 million tons of woody biomass is produced. Currently, there are nearly 100,000 acres of hybrid poplars growing in the Pacific Northwest.
- Can be harvested with short rotations

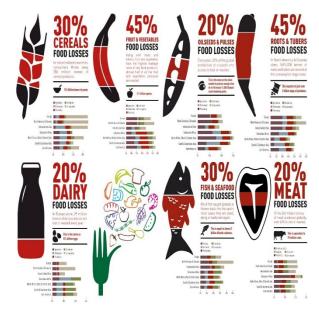




## Softwood (e.g. D. Fir)

- 8.1 million tons forest residues biomass produced in WA alone.
- On the commercial timberlands of the western region, there are approximately 14 million hectares of Douglas fir managed primarily in natural stands.





#### **Food Processing Waste**

Courtesy: https://makanaka.wordpress.com/tag/foodwaste/



#### **Manure**

• USDA estimates more than 335 million tons of "dry matter" waste is produced annually on farms in the United States. More than 1.9 million tons animal waste in WA.

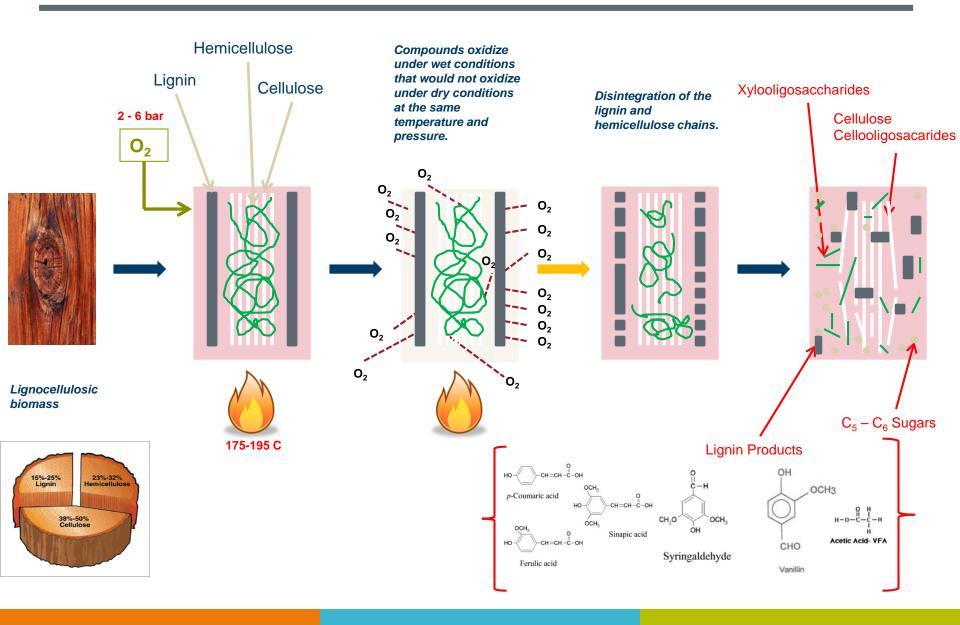
## Why is Pretreatment Needed?

- Biomass recalcitrance requires pretreatment
- Pretreatment is the most costly process step: the only process step more expensive than pretreatment is no pretreatment
  - Low yields without pretreatment drive up all other costs more than amount saved
  - Enhancing yields via improved pretreatment would reduce all other unit costs
- Lowering cost of pretreatment makes biorefineries more viable
- Making full use of the biomass raw materials allows for improved economy
- What you add of chemicals during pretreatment will stay around and set limits for the full use of the biomass

## **Biomass Pretreatment Technologies**

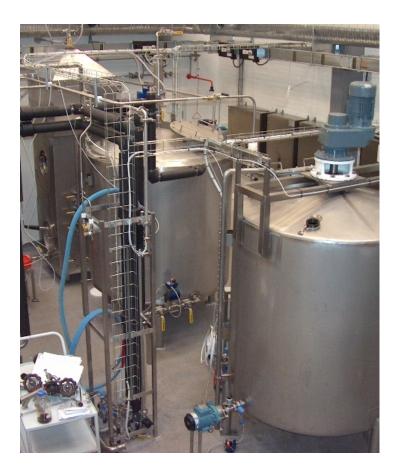
- Size reduction (comminution)
- Low pH (acid)
  - Dilute acid, SO<sub>2</sub>, etc.
- Neutral pH (water)
  - Autohydrolysis, controlled pH
- High pH (alkaline)
  - · Lime, liquid ammonia soaking, AFEX, etc.
- Organic solvent
  - Organosolv, COSLIF, etc.
- Ionic liquids (ILs)
- Biological

## **WET OXIDATION**





## Pilot plant



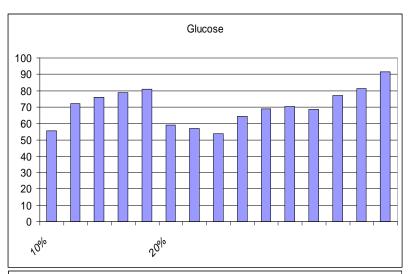


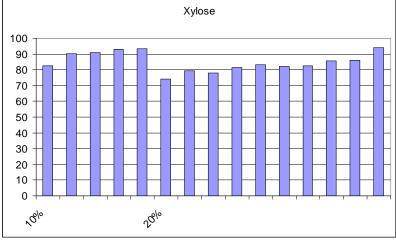




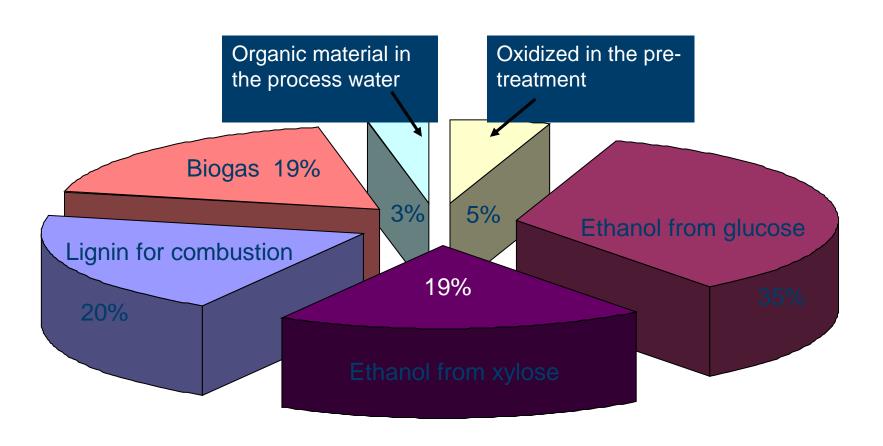








## Optimized use of the biomass

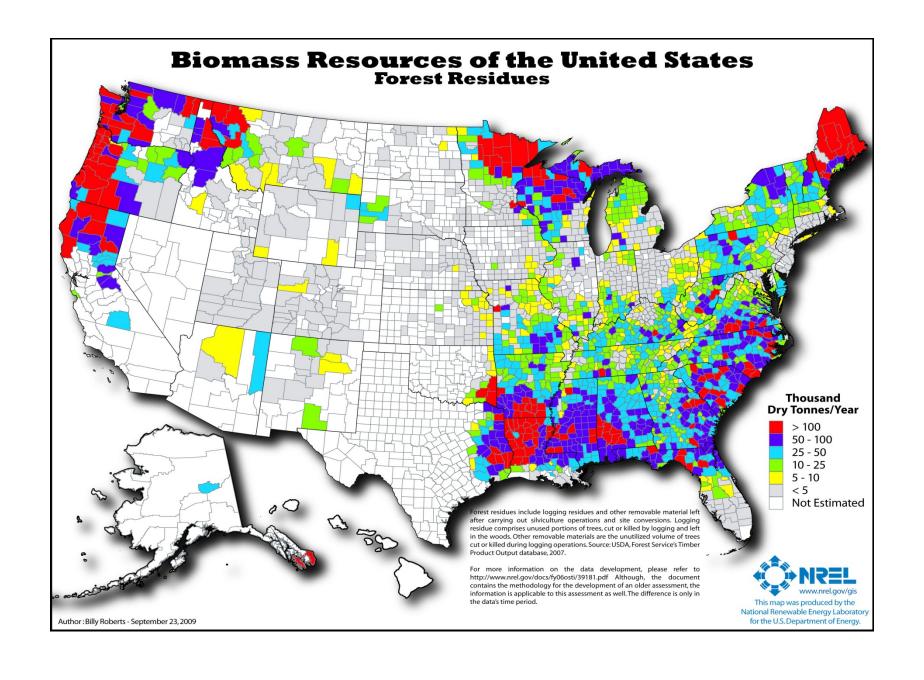


## **Conclusions Ag Waste**

- Wet explosion gave high sugar yields even with high solids loading
- With the newest development of AWEx and cellulosic enzymes we can run the process at 30% DW with over 90% sugar yield
- New results in our lab has shown that on-site produced enzymes can substitute commercial enzymes and result in a significant lowering of enzyme cost

## Forest slash: Opportunities and problems for turning Slash to Cash!

- What is it: Tops, stumps, leaves and needles that are removed during trunk stripping.
- What is the opportunity: Slash tallies 16% of logging activities in the USA resulting in 49 million tons in 2004, according to the U.S. Department of Energy.
- Current slash management includes on site burning, chipping and/or collection at the sides of roads for later pickup and combustion.
- What is the problem: Forest slash is bulky, low-density material, usually located in remote logging areas. This abundant, essentially free feedstock can be too expensive to collect and transport.





### Downsizing on the logging spot

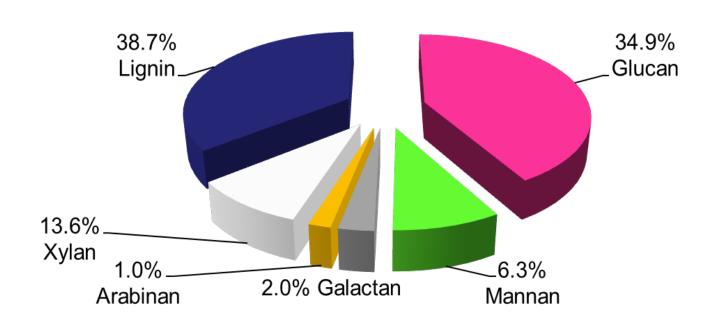


Down-sizing before use for combustion



## Douglas fir (FS-03) Composition of washed material

Loblolly Pine



## Softwood to Hydrolysate and Sugars



Milling





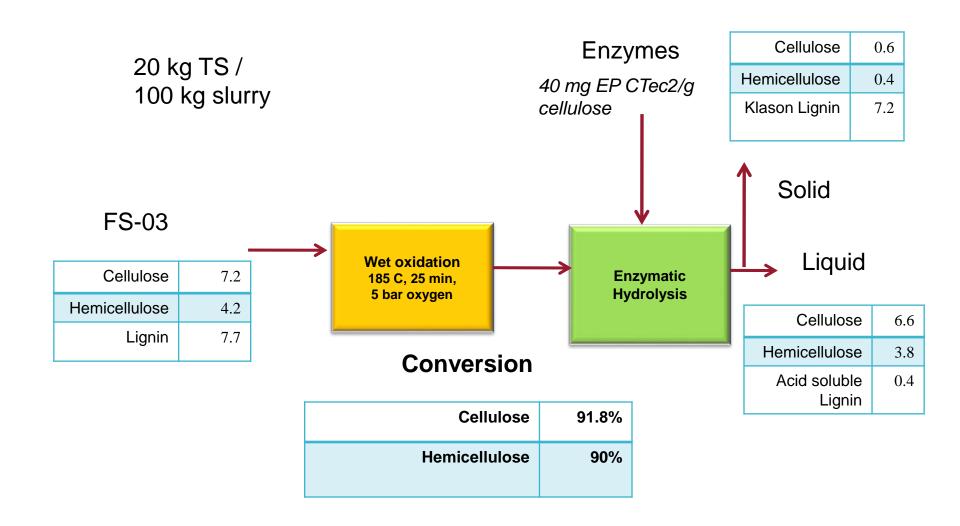


Pretreatment



Hydrolysis

## MASS BALANCE – Douglas fir (FS-03)



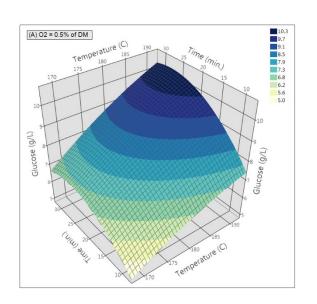
**Table 1** Experimental design of the wet explosion pretreatment of Douglas fir FS-10 samples in pilot-scale at 30% dry matter.

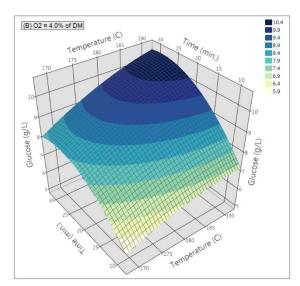
| Run          | Pattern | Temp., °C (T) | O <sub>2</sub> , % DM | Time, min. (t) |
|--------------|---------|---------------|-----------------------|----------------|
| 1            |         | 170           | 0.5                   | 10             |
| 2            | _+_     | 170           | 7.5                   | 10             |
| 3            | a00     | 170           | 4.0                   | 20             |
| 4            | +       | 170           | 0.5                   | 30             |
| 5            | _++     | 170           | 7.5                   | 30             |
| 6            | 00a     | 180           | 4.0                   | 10             |
| 7            | 0a0     | 180           | 0.5                   | 20             |
| 8 (central)  | 000     | 180           | 4.0                   | 20             |
| 9 (central)  | 000     | 180           | 4.0                   | 20             |
| 10 (central) | 000     | 180           | 4.0                   | 20             |
| 11           | 0A0     | 180           | 7.5                   | 20             |
| 12           | 00A     | 180           | 4.0                   | 30             |
| 13           | +       | 190           | 0.5                   | 10             |
| 14           | ++_     | 190           | 7.5                   | 10             |
| 15           | A00     | 190           | 4.0                   | 20             |
| 16           | +_+     | 190           | 0.5                   | 30             |
| 17           | +++     | 190           | 7.5                   | 30             |

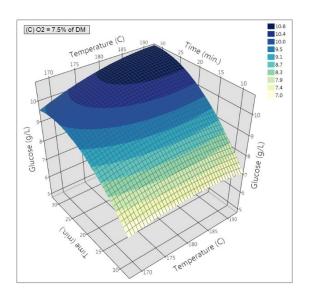
Optimization of process conditions



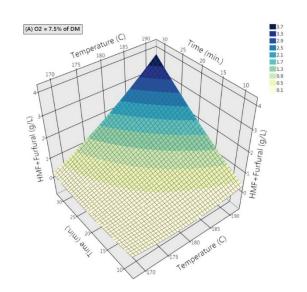
Mass balance closure of the cellwall components

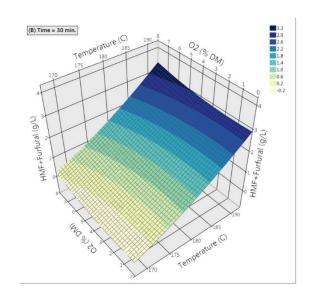


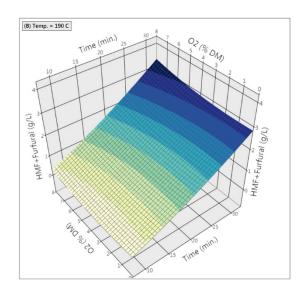




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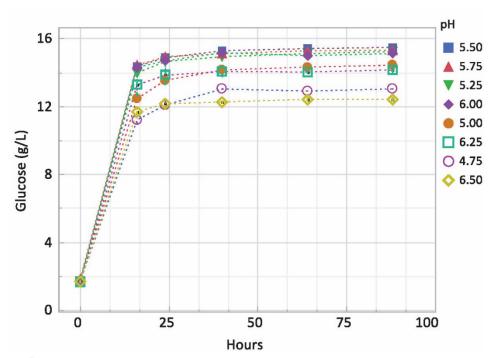
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#### **Enzymes used:**

Mixture of Cellic® CTec2 and Cellic® HTec2

#### **Enzyme dosage:**

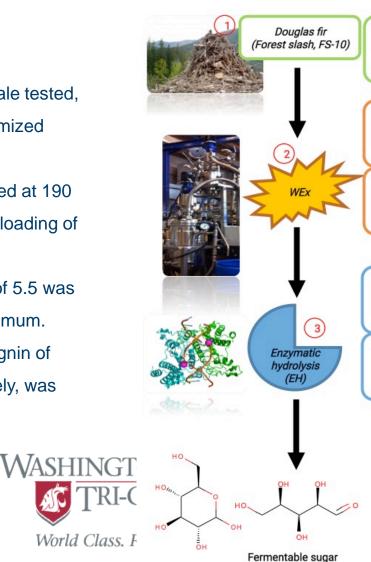
16 mg enzyme proteins (EP)/g PFS-10 (oven dry basis, of which 14 mg EP from CTec2 and 2mg EP from HTec2)



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#### **Highlights**

- The wet explosion at pilot-scale tested, process conditions were optimized using DOE.
- Maximum digestibility achieved at 190
   °C, time 30 min, and oxygen loading of 7.5%.
- Glucose yield at optimal pH of 5.5 was
   63.3% of the theoretical maximum.
- A recovery of cellulose and lignin of 99.9% and 96.3%, respectively, was achieved.



100.0 kg dry weight

30.45 kg Glucan (100%) 2.18 kg Galactan (100%) 8.86 kg Mannan (100%) 5.42 kg Xylan (100%) 1.36 kg Arabinan (100%) 46.47 kg Lignin (100%)

#### 69.51 kg insoluble solids

17.60 kg Glucan (57.8%) 0.16 kg Galactan (7.3%) 0.64 kg Mannan (7.2%) 0.49 kg Xylan (9.1%) 0.04 kg Arabinan (2.6%) 53.2 kg Lignin (114.5%)

#### 430.49 kg liquid with soluble solids\*

9.56 kg Glucose (28.3%) <sup>a</sup> 3.72 kg Xylose (60.5%) <sup>b</sup> 2.81 kg Galactose (116.4%) <sup>c</sup> 1.36 kg Arabinose (88.1%) <sup>d</sup> 6.83 kg Mannose (69.4%) <sup>e</sup> 0.12 kg Lignin (0.3%)

\*Of which oligomeric form: a) 18%; b) 50%; c) 64%; d) 4%; e) 70%

#### 55.51 kg insoluble solids

11.16 kg Glucan (36.6%) 0.05 kg Galactan (2.5%) 0.42 kg Mannan (4.7%) 0.26 kg Xylan (4.8%) 0.04 kg Arabinan (2.8%) 44.62 kg Lignin (96.0%)

#### 444.49 kg liquid with soluble solids\*\*

21.38 kg Glucose (63.3%) <sup>a</sup> 3.96 kg Xylose (64.4%) <sup>b</sup> 2.38 kg Galactose (88.3%) <sup>c</sup> 1.36 kg Arabinose (88.3%) <sup>d</sup> 7.02 kg Mannose (71.3%) <sup>e</sup> 0.11 kg Lignin (0.2%)

\*\*Of which oligomeric form: a) 0%; b) 4%; c) 12%; d) 13%; e) 9%

#### Fermentable sugar yields after EH (%)

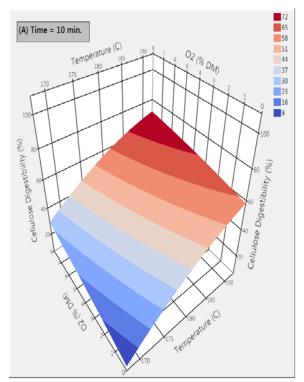
Glucose (63.3%) Xylose (64.4%) Galactose (98.4%) Arabinose (88.3%) Mannose (71.3%) Recovery (%) Glucan (99.9%) Xylan (69.2%) Galactan (100.9%) Arabinan (91.1%) Mannan (76.0%) Lignin (96.3%)

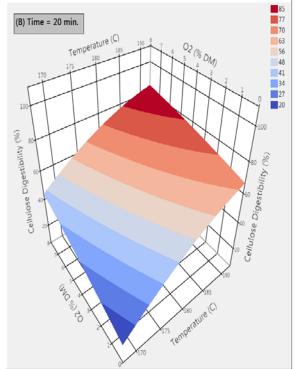
## COMPARING SUGAR YIELDS FROM SOFTWOOD

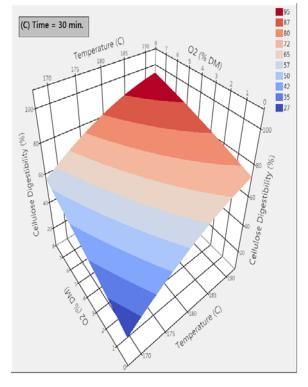
| Type of Biomass         | Type of<br>Pretreatment         | Pretreatment<br>Temperature (°C)-Time (min)                                       | Enzymatic<br>Hydrolysis | Theoretical<br>Yield<br>(Total Sugars) | Reference                      |
|-------------------------|---------------------------------|---|-------------------------|--|--------------------------------|
| Softwood                | Two- step Steam<br>Pretreatment | Stage 1: 190-2, 3% <b>SO<sub>2</sub></b> Stage 2: 220-5, 3% <b>SO<sub>2</sub></b> | 2% DM                   | 80%                                    | Söderström J. et al.<br>(2002) |
| Pinus rigida            | Organosolv                      | 210-10, 1% <b>MgCl</b> <sub>2</sub>   | 1% DM                   | 75.88%                                 | Park N. et al. (2010)          |
| Bettle Killed Lodgepole | One step Steam<br>Pretreatment  | 200-5, 4% <b>SO</b> <sub>2</sub>  | 2% DM                   | 75%                                    | Ewanick S. et al. (2007)       |
| DF (FS-03)              | Wet oxidation                   | 185-25, 5 bar <b>O</b> ₂  | 20% DM                  | 90-92%                                 | This study                     |

## Bioprocessing of poplar sawdust

Up to 90% of sugar production as monomers

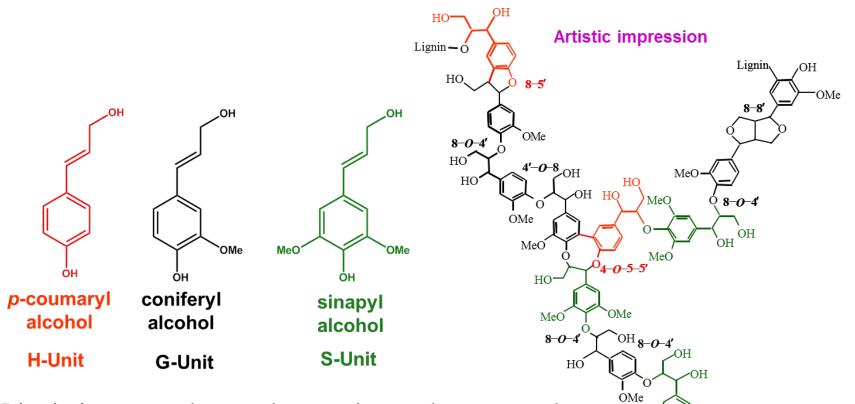






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• Lignins are formed by oxidative radical-radical coupling using three main monolignols.



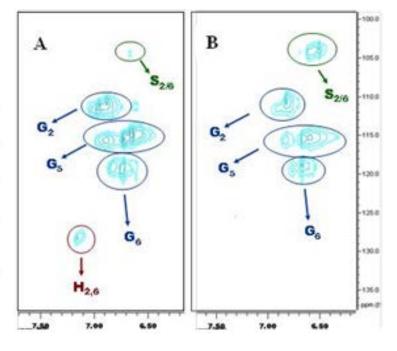
MeO

OMe

• Lignin is a natural amorphous polymer that acts as the essential glue that gives plants their structural integrity. The current vision undervalues lignin's potential to address production of high value and commodity products. An attractive alternative is valorization of lignin for conversion to value added products.

## **Wet Exploded Lignin**

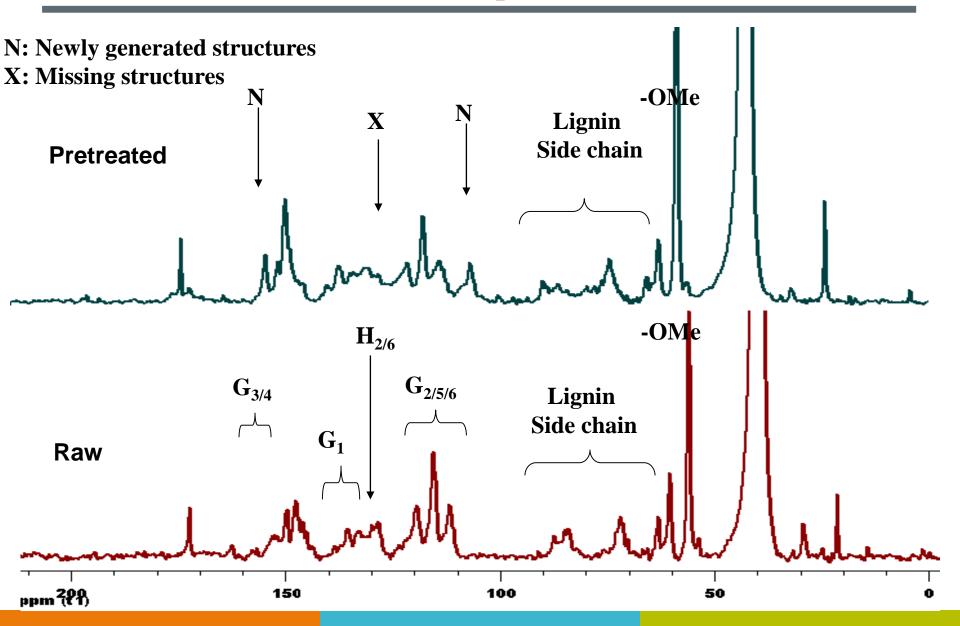
| Sample                               | %C   | % H | % N  | % O  | % S   |
|--------------------------------------|------|-----|------|------|-------|
| Forest Residual Lignin               | 61   | 6.0 | 0.07 | 32.9 | 0.032 |
| Wet Exploded Lignin                  | 64.9 | 5.3 | 0.96 | 28.7 | 0.096 |
| Mild Bisulfite<br>Lignosulfonic acid | 52.1 | 4.8 | 0.36 | 34.7 | 8.10  |



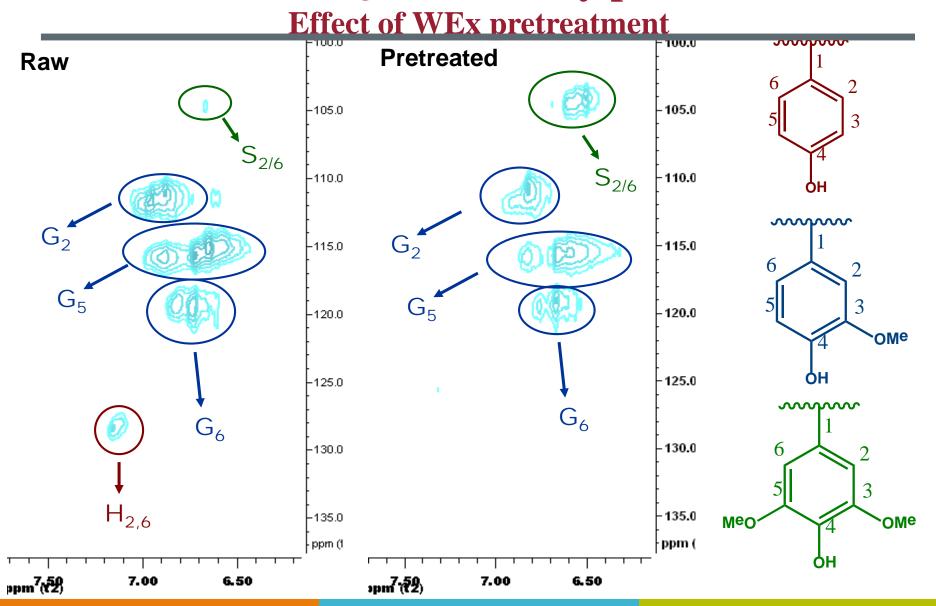
- Initial studies were done on both Douglas Fir and Loblolly Pine lignin after wet explosion pretreatment at optimized conditions for sugar recovery.
- Studies showed that wet explosion pretreatment increased amount of methylated compounds (S- & G- units) which reduced recondensation and repolymerization of lignin after cooling.
- Wet explosion pretreatment also showed higher Carbon concentration when compared to lignosulphonates.

## <sup>13</sup>C NMR of loblolly pine

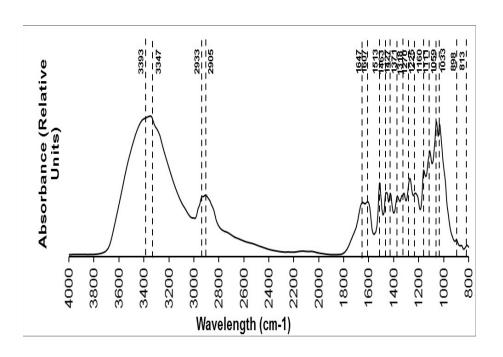
**Effect of WEx pretreatment** 



## 2D Heteronuclear Single Quantum Coherence (HSQC)of loblolly pine



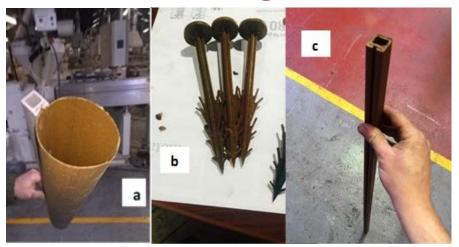
### FTIR Analysis of Wet Exploded FS-10 Lignin



| Observed Peak<br>Maximum (cm <sup>-</sup> | Peak Assignment                           |
|---|---|
| 1)  |   |
| 3347, 3393                                | O-H stretch (hydrogen bonded)             |
| 2905, 2933                                | C-H stretching of methyl and methylene    |
|   | groups                                    |
| 1647                                      | Adsorbed O-H, conjugated C=O              |
|   | (cellulosic)                              |
| 1607                                      | C=C stretching of aromatic ring in lignin |
| 1513                                      | Aromatic skeletal vibrations              |
|   | (guaiacyl>syringyl)                       |
| 1463                                      | C-H bending of methyl and methylene       |
|   | groups                                    |
| 1427                                      | C-H deformation in lignin                 |
| 1371                                      | C-H deformation symmetric (cellulosic);   |
|   | Phenolic OH (lignin)                      |
| 1318                                      | CH <sub>2</sub> wagging (cellulosic)      |
| 1270                                      | C-O stretching of guaiacyl unit           |
| 1225                                      | C-C, C-O and C=O stretching of            |
|   | guaiacyl unit                             |
| 1160                                      | C-O-C asymmetric vibration (cellulosic)   |
| 1111                                      | Aromatic C-H deformation of syringyl      |
|   | units                                     |
| 1059                                      | C-O stretching of secondary               |
|   | alcohols/cellulosic                       |
| 1033                                      | C-O stretching of primary alcohols        |
| 898                                       | C-H deformation vibration of cellulose    |
| 813                                       | C-H bending of syringyl units             |

- FTIR analysis indicated greater amount of guaiacyl (G-) components in the biorefinery lignin when compared to syringyl (S-) or hydroxyphenyl (H-) components with an S/G ratio of 0.811 (obtained from comparing FTIR absorbance at 1270 cm<sup>-1</sup> and 1225 cm<sup>-1</sup>.
- These studies also showed that linkages related to both softwood and hardwood biomass was found in FS-10 (softwood being more prominent)

## **Lignin-Based Products**



Different reinforced PLA products produced from WEx-treated lignin at 20 wt% loading (a) tree sapling protector attached to a stake; (b) pegs; (c) stake.

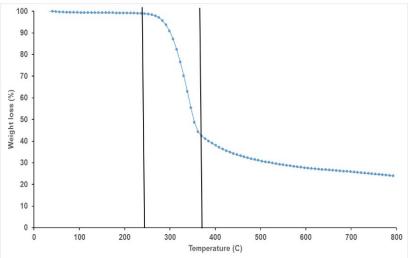
- These products were made in collaboration with Greener Polymers LLC for forestry applications.
- Currently, other biodegradable plastics for common household applications such as paper cups, coffee lids, paper plates etc. are being produced using WEx Lignin-reinforced PLA.
- These products were found to have superior mechanical properties compared to natural wood fibers and required less additives due to aromatic nature of the WEx Lignin. 20% Blending with PLA also showed cost savings.

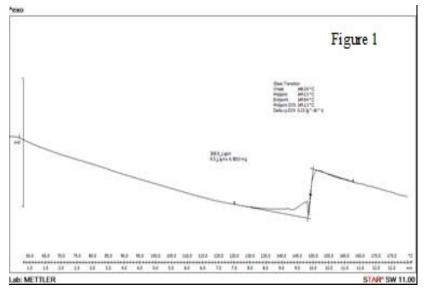
## **Carbon Fibers from WEx Lignin**





- Current work is being done in modifying WEx biomass lignin for carbon fiber production.
- The research is being done in conjunction with companies such as Ford and Hyundai in increasing lignin reinforcement in carbon fibers using different environmentally-benign and low-cost techniques.





### **Other Products**

- Srinivas, K., Oliveira, F. D. C., Teller, P., Gonclaves, A. R. and Ahring, B. K., 2015, Characterization and oxidative degradation of biorefinery lignin obtained from pretreated forest residues of Douglas Fir, Manuscript submitted.
- Srinivas, K., Oliveira, F. D. C., Teller, P., Gonclaves, A. R. and Ahring, B. K., 2015, Characterization and optimization of alkaline wet oxidation of biorefinery lignin obtained from pretreated forest slash, Pacifichem, Honolulu, Hawaii, December 15-20.
- Rana, D., Laskar, D. D., Srinivas, K. and Ahring, B. K. 2015, Wet explosion pretreatment of loblolly pine leads to an increase in methoxylation of the lignin, Bioresour. Bioprocessing, 2, 26, doi: 10.1186/s40643-015-0054-8.

### CONCLUSION

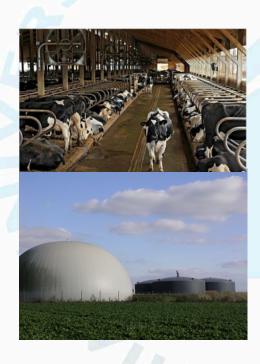
- Wet oxidation was found to be a well suited pretreatment method for forest slash (softwood)
- Wet oxidation was further found to produce high sugar yields (both C6 and C5) from both softwood and hardwood
- Fermentation tests showed no inhibition with up to 25% hydrolysate with both bacteria and fungal biocatalysts
- Investigation of the lignin modification during wet oxidation pretreatment show that the pretreatment results in significant changes to the lignin structure
- The decrease in highly condensed lignin structure resulting from wet oxidaton might increase the cellulose accessability, thus decrease the need for enzymes and further increase the value of the lignin for producing high-value lignin products
- The pure lignin produced as a result of AWEx makes the material suitable as raw material for high-value bioplastics

## AD of manure

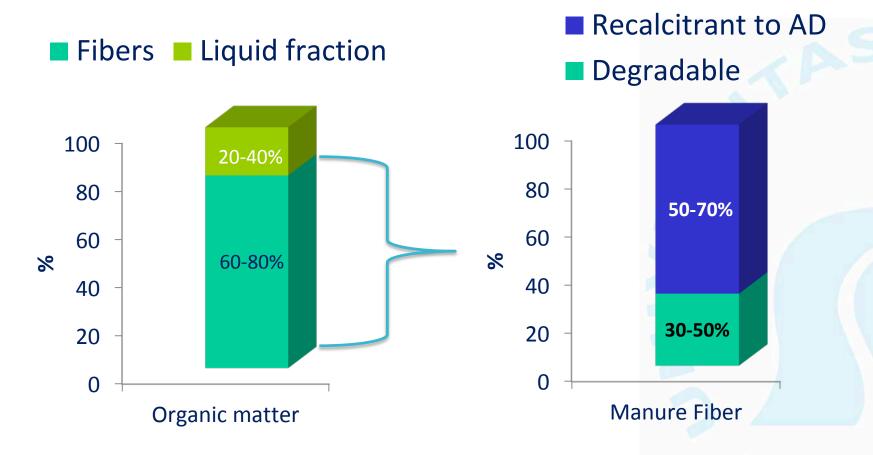
Biogas production from manure has the highest reduction effect on greenhouse gas emissions

#### **Key Focus Areas:**

- ➤ Yield, < 25 m³ biogas/m³ manure
- Fibers of manure is recalcitrant to AD
- Economic operation, yield > 30 m³ biogas/m³ manure required.
- Reduce the dependency on limited amount of high biogas potential industrial organic waste.



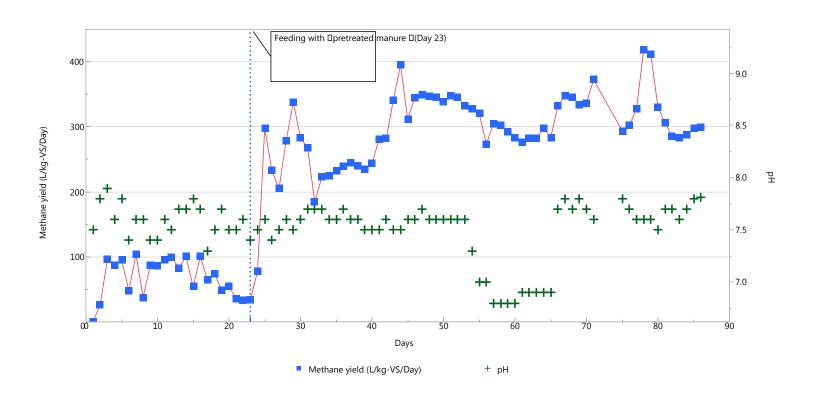
## AD of manure



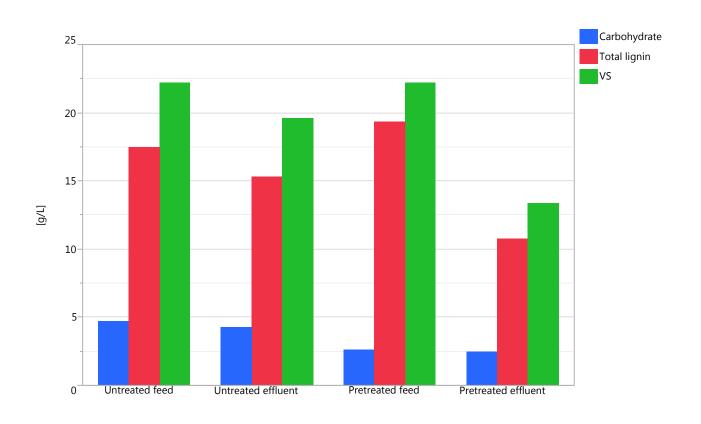
Organic matter distribution in manure slurry

Degradability of manure fiber in traditional AD

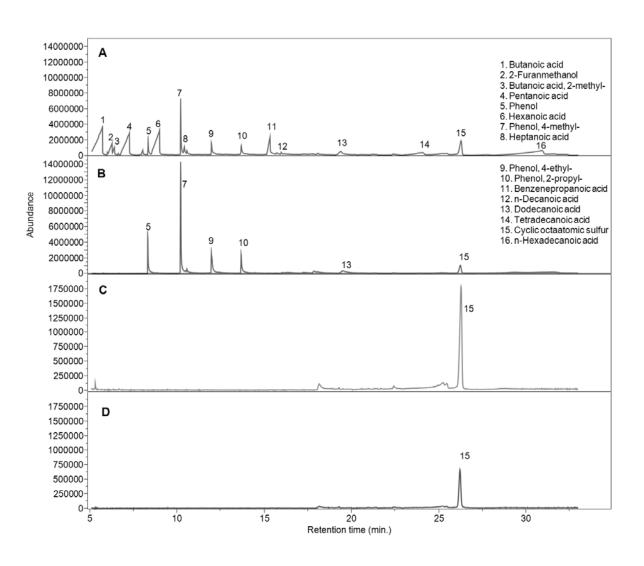
## Methane from lignin-enriched manure after AWEx



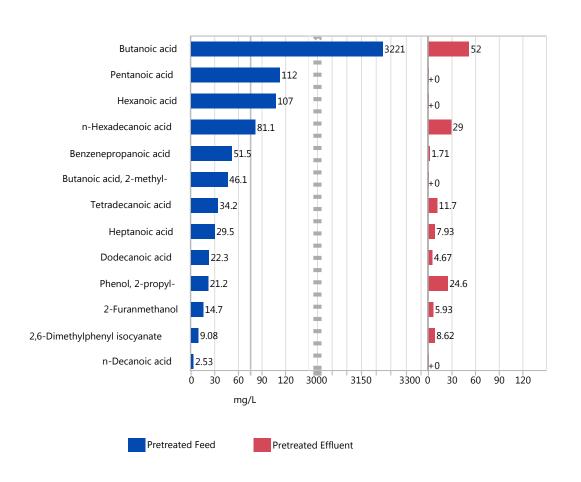
## Lignin conversion in AD after AWEx



## Wet explosion of feedlot manure



## Wet explosion of feedlot manure



| Raw Material                     | Methane Yield<br>(I CH4/ g VS) | Gas Increase (%) |
|----------------------------------|--------------------------------|------------------|
| Woody yard waste                 | 0.35                           |                  |
| Same with AWEx                   | 0.69                           | 97%              |
| Food waste                       | 0.54                           |                  |
| Same with AWEx                   | 0.57                           | 6%               |
| AD-digested Biowaste (yard/food) | 0.19                           |                  |
| Same with AWEx                   | 0.37                           | 95%              |
| AD-digested sewage sludge        | 0.16                           |                  |
| Same with AWex                   | 0.32                           | 100%             |

vvoria Ciass, race to race.

## <sup>2</sup> Conclusion manure/AD:

- CH<sub>4</sub> yield from manure can be significantly improved using the AD-Booster concept.
- ❖ CSTR expt. shows between 50 and 300 % higher CH₄ yield when the fibers are treated by AWEx after AD
- Addition AWEx pretreated lignocellulosic biomass materials could change the economics of biogas production
- ❖ The first industrial scale AD-Booster (4 ton per hour) continuous plant is currently being implemented in Europe in connection to a large centralized biogas plant